

Effect of Heat and Mass Transfer on Unsteady Convective MHD Couette Flow through Porous Medium with Oscillating Temperature.

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ABSTRACT

The effect of heat and mass transfer on unsteady free convection oscillatory flow through parallel flat plates in a porous medium with heat source and chemical reaction is investigated with free stream Velocity, temperature and concentration oscillate in time about a non-zero constant mean. A closed form analytical solution is obtained by adopting regular perturbation method to solve the momentum and energy and concentration equations. Effect of various non-dimensional parameters on velocity, temperature and concentration profiles have been analysed in detail and results are shown in graphs.

Keywords: MHD, Natural Convection, Couette flow, Oscillatory, porous medium, heat and mass transfer.

Introduction

The study of free convective fluid flow is a classical investigation in the field of flow of fluids and thermal variations and conduction. These studies significantly involved in various industrial applications like nuclear power plant, solid matrix heat transfer, porous smooth plate receivers, oil retrieval, distributing and diffusing chemical wastes in various practices, dispersing nuclear discarded material, grains preservation and aeration and much more. Furthermore, free convective flow has a great influence in the field of solar heating systems and is widely used in ventilating passive system. As there are numerous interests, research developments and analysis in free-convective flow, there are many studies in MHD free convection flows in various surfaces with different phenomena. With the effect of heat transfer and the radiation effect of MHD flow influenced by the magnetic field also of interest in various application areas such as space technology, nuclear power plants, temperature changes in transmission lines, electric transformers etc.

Heinisch et al. [1] studied transient free convection flow in laminar boundary layer equations using an integral technique. He arrived at a solution by solving a system of PDE with two independent variables and ODE with two different methods. Hossain et al. [2] considered a vertical thin cylinder with the flow of natural convection radiation interaction with boundary layer and further he investigated the same for conduction radiation interaction using finite difference method in which the fluid is incompressible over an isothermal horizontal plate [3]. Mina et al. [4] studied unsteady free convection flow in moving sheet with ambient fluid. He applied group theoretic approach in which a constant insulated plate influenced the thermal boundary layer in a vertical layer of Boussinesq fluid. Makinde [5] investigated convective flow, energy emission and molecular transport together with assumption plate travels in the plane which is kept in fixed temperature with constant elements concentration, considered the grey fluid with absorption and emission and found solution corresponding to the equations pertaining to nonlinear thrust, energy and deliberation. Mehmet et al. [6] considered the vertical down point cone to study the effect of laminar free convection flow influenced with the magnetic field, found its energy and flow rate distribution for various parameter values. Kassem et al. [7] found a solution for stability in convective flow of a plate moves vertically influenced with a constant heat variation.

As micro polar fluid has a variety of applications and is important in the study of suspended particles, Prathap et al. [8] had taken two different regions to analyse the laminar free convection flow in which one is occupied by micro polar fluid and the other one by a viscous fluid, found the expressions as analytic solution for velocity, temperature and the velocity corresponds to the micro rotation. Basant et al. [9] studied the flow of hydro dynamics with thermal

characteristics of viscous reactive fluids transient free convection flow and dimensionless parameters are employed insolving the governing equations.

MamunMollaa et. al. [10] studied with streamwise sinusoidal surfacetemperature which the viscous incompressible optically thick fluids natural convectionlaminar flow with the effect of thermal radiation in two dimension has been analysed.Ali et. al. [11] analysed it with a vertical plate influenced with Joule heating and its thermal effect by employing dimensionless parameters with suitable transformations using Keller box scheme and FEM. Nazma et. al. [12] analysed with the same method to find the effect of energy conduction on natural convection along oscillatory plate. Mahesha et. al. [13] had analysed the cross diffusion and double diffusive convection effect of a vertically spinning cone with the effect of magnetic field having the application in oceanography. Ruthra et. al. [14] considered the motion of incompressible fluid with rotational cylinder to study the effect of this flow assuming the cylinder starts spontaneously with constant acceleration corresponds to the rotating fluid. Abdul et. al. [15] analysed the flow in a square cavity influenced by the magnetic field and with different temperature sources.

The aim of this chapter is to analyse the problem of radiating MHD oscillatory flow. Fluid is assumed to be flowing through two parallel plates in a porous structure. When the buoyancy forces react with the flow fluid as free convective flow, the effect of magnetic field which influence the thermal radiation has been analysed with freestream velocity, concentration and temperature profiles. This problem has not been reported earlier in the literature.

Mathematical Modelling

The problem of MHD oscillatory Couette flow of a viscous incompressible fluid is considered. It is assumed that fluid is finitely conducting and flowing between two parallel plates enclosing permeable structure. One plate is suddenly moved with free stream flow rate U^* that assumed to be oscillating about mean. Choosing the coordinate axes in the directions along the plate vertically and normal to that plate respectively.

The governing equations of the flow are formulated from Navier-Stokes equation and Maxwell's equation for MHD with the assumptions that magnetic force is taken normal to the boundaries and the induced magnetic field is neglected. The governing equations of the flow are:

$$\frac{\partial u^*}{\partial t^*} = \frac{\partial U^*}{\partial t^*} + \nu \frac{\partial^2 U^*}{\partial y^{*2}} + g\beta_T(T^* - T_b^*) + g\beta_C(C^* - C_b^*) - \left(\frac{\bar{J} \times \bar{B}}{\rho}\right) - \frac{\nu u^*}{k^*} - \frac{1}{\rho} \frac{\partial p^*}{\partial x^*} \quad (1)$$

Where $\bar{J} \times \bar{B} = \sigma(\bar{v} \times \bar{B}) \times \bar{B}$, then $\left(\frac{\bar{J} \times \bar{B}}{\rho}\right) = \frac{(u^* - U^*)\sigma B^2}{\rho}$ and hence equation (3.1) becomes

$$\frac{\partial u^*}{\partial t^*} = \frac{\partial U^*}{\partial t^*} + \nu \frac{\partial^2 U^*}{\partial y^{*2}} + g\beta_T(T^* - T_b^*) + g\beta_C(C^* - C_b^*) - \left(\frac{(u^* - U^*)\sigma B^2}{\rho}\right) - \frac{\nu u^*}{k^*} - \frac{1}{\rho} \frac{\partial p^*}{\partial x^*} \quad (2)$$

$$\frac{\partial T^*}{\partial t^*} = \alpha \frac{\partial^2 T^*}{\partial y^{*2}} + Q^*(T^* - T_b^*) \quad (3)$$

$$\frac{\partial C^*}{\partial t^*} = D \frac{\partial^2 C^*}{\partial y^{*2}} - K_r^*(C^* - C_b^*) \quad (4)$$

The corresponding BCs are given by

$$\left. \begin{aligned} \text{At } y^* = 0, u^* = U_0(1 + \varepsilon e^{i\omega^* t^*}), T^* = T_0^* + \varepsilon(T_0^* - T_b^*)e^{i\omega^* t^*}, C^* = C_0^* + \varepsilon(C_0^* - C_b^*)e^{i\omega^* t^*}, \\ \text{At } y^* = b, u^* = 0, T_0^* = T_b^*, C_0^* = C_b^* \end{aligned} \right\} \quad (5)$$

Transforming the dimensional quantities as

$$\left. \begin{aligned} \bar{u} = \frac{u^*}{U_0}, \bar{t} = \omega^* t^*, \omega = \frac{\omega^* b^2}{\nu}, \theta = \frac{T^* - T_b^*}{T_0^* - T_b^*}, Gr = \frac{g\beta b^2(T_0^* - T_b^*)}{\nu U_0}, Q = Q^* \frac{b^2}{\alpha}, \\ \bar{y} = \frac{y^*}{b}, Gc = \frac{g\beta_C b^2(C_0^* - C_b^*)}{\nu U_0}, \phi = \frac{C^* - C_b^*}{C_0^* - C_b^*}, K = \frac{b^2 U_0}{\nu^2} K_r^*, Sc = \frac{\nu}{D}, M = \sqrt{\frac{\sigma B^2 b^2}{\rho \nu}}, Pr = \frac{\nu}{\alpha} \end{aligned} \right\} \quad (6)$$

Using equation (6), governing equations in non-dimensional form obtained as

Momentum equation:

$$\omega \left(\frac{\partial \bar{u}}{\partial \bar{t}} - \frac{\partial U}{\partial \bar{t}} \right) = \frac{\partial^2 \bar{u}}{\partial \bar{y}^2} + Gr\theta + Gc\phi - (s^2 + M^2)\bar{u} + M^2 U \quad (7)$$

Energy equation:

$$\omega Pr \frac{\partial \theta}{\partial t} = \frac{\partial^2 \theta}{\partial y^2} + Q\theta \quad (8)$$

Concentration equation:

$$\omega \left(\frac{\partial \phi}{\partial t} \right) = \frac{1}{Sc} \frac{\partial^2 \phi}{\partial y^2} - K\phi \quad (9)$$

With the boundary conditions

$$\left. \begin{aligned} y = 0, u = 1 + \varepsilon e^{it}, \\ y = 1, u = \theta = C = 0 \end{aligned} \right\} \quad (10)$$

Solution by Regular Perturbation Method

Due to small variation $\varepsilon (<< 1)$ in all the flow profiles, the solutions can be taken as :

$$u(y, t) = u_0(y) + \varepsilon u_1(y) e^{it} \quad (11)$$

$$\theta(y, t) = \theta_0(y) + \varepsilon \theta_1(y) e^{it} \quad (12)$$

$$\phi(y, t) = \phi_0(y) + \varepsilon \phi_1(y) e^{it} \quad (13)$$

and for free stream velocity

$$U = 1 + \varepsilon e^{it} \quad (14)$$

Substituting equations (11) – (14) in equations (7) – (9), the governing equations become

Temperature equation:

$$(\theta_0'' + Q\theta_0) = 0 \quad (15)$$

$$(\theta_1'' - (Q - Pr i \omega)\theta_1) = 0 \quad (16)$$

Concentration equation:

$$(\phi_1'' - (KSc - i\omega Sc)\phi_1) = 0 \quad (17)$$

$$\phi_0'' - ScK\phi_0 = 0 \quad (18)$$

Momentum equation:

$$u_0'' - (s^2 + M^2)u_0 = -(Gr\theta_0 + Gc\theta_0 + M^2) \quad (19)$$

$$u_1'' - (s^2 + M^2 + i\omega)u_1 = -Gr\theta_1 - Gc\theta_1 + (i\omega + M^2) \quad (20)$$

With the corresponding BCs

$$\left. \begin{aligned} y = 0, u_0 = 1, u_1 = 1, \theta_0 = 1, \theta_1 = 1, \phi_0 = 1, \phi_1 = 1, \\ y = 1, u_0 = 0, u_1 = 0, \theta_0 = 0, \theta_1 = 0, \phi_0 = 0, \phi_1 = 0 \end{aligned} \right\} \quad (21)$$

Solving (15) and (16),

$$\theta_0 = a_{01} e^{n_3 y} + a_{12} e^{-n_3 y} \quad (22)$$

$$\theta_1 = a_{11} e^{n_2 y} + a_{12} e^{-n_2 y} \quad (23)$$

Solving (17) and (18),

$$\phi_0 = b_{01} e^{n_5 y} + b_{02} e^{-n_5 y} \quad (24)$$

$$\phi_1 = b_{11} e^{n_4 y} + b_{12} e^{-n_4 y} \quad (25)$$

Solving (19),

$$C.F. = c_{01} e^{n_7 y} + c_{02} e^{-n_7 y}$$

$$P.I_1 = \frac{1}{(D^2 - n_7^2)} (-Gr \theta_0) = \frac{1}{(n_3^2 - n_7^2)} (-Gr \theta_0)$$

$$P.I_2 = \frac{1}{(D^2 - n_7^2)} (-Gc \phi_0) = \frac{1}{(n_5^2 - n_7^2)} (-Gc \phi_0)$$

$$\therefore u_0 = c_{01} e^{n_7 y} + c_{02} e^{-n_7 y} - \frac{Gr \theta_0}{(n_3^2 - n_7^2)} - \frac{Gc \phi_0}{(n_5^2 - n_7^2)} + \left(\frac{M^2}{n_7^2} \right) \quad (26)$$

Solving (20), $C.F. = c_{11} e^{n_6 y} + c_{12} e^{-n_6 y}$

$$\begin{aligned} P.I_1 &= \frac{1}{(D^2 - n_6^2)} (-Gr \theta_1) = \frac{1}{(n_2^2 - n_6^2)} (-Gr \theta_1) \\ P.I_2 &= \frac{1}{(D^2 - n_6^2)} (-Gc \phi_1) = \frac{1}{(n_4^2 - n_6^2)} (-Gc \phi_1) \\ \therefore u_1 &= c_{11} e^{n_6 y} + c_{12} e^{-n_6 y} - \frac{Gr \theta_1}{(n_2^2 - n_6^2)} - \frac{Gc \phi_1}{(n_4^2 - n_6^2)} + \left(\frac{M^2 + i\omega}{s^2 + M^2 + i\omega} \right) \end{aligned} \quad (27)$$

The velocity, temperature and concentration distributions are obtained as

$$\begin{aligned} u(y, t) &= (c_{01} e^{n_7 y} + c_{02} e^{-n_7 y}) - \frac{Gr \theta_0}{(n_3^2 - n_7^2)} - \frac{Gc \phi_0}{(n_5^2 - n_7^2)} + \left(\frac{M^2}{n_7^2} \right) \\ &+ \varepsilon \left[(c_{11} e^{n_6 y} + c_{12} e^{-n_6 y}) - \frac{Gr \theta_1}{(n_2^2 - n_6^2)} - \frac{Gc \phi_1}{(n_4^2 - n_6^2)} + \left(\frac{M^2 + i\omega}{s^2 + M^2 + i\omega} \right) \right] e^{it} \end{aligned} \quad (28)$$

$$\theta(y, t) = a_{01} e^{n_3 y} + a_{02} e^{-n_3 y} + \varepsilon [a_{11} e^{n_2 y} + a_{12} e^{-n_2 y}] e^{it} \quad (29)$$

$$\phi(y, t) = b_{01} e^{n_5 y} + b_{02} e^{-n_5 y} + \varepsilon [b_{11} e^{n_4 y} + b_{12} e^{-n_4 y}] e^{it} \quad (30)$$

The skin friction, rate of heat transfer and mass transfer are obtained as

$$\tau = \left\{ \frac{\partial u}{\partial y} \right\}_{y=h_1, h_2}$$

$$\tau = \varepsilon [e^{ti+n_6 y} c_{11} n_6 - e^{ti-n_6 y} c_{12} n_6] + c_{01} n_7 e^{n_7 y} + c_{02} n_7 e^{-n_7 y}$$

$$- \left[\frac{Gr}{(n_3^2 - n_7^2) \frac{\partial \theta_0}{\partial y} \frac{Gc}{(n_5^2 - n_7^2) \frac{\partial \phi_0}{\partial y}} \frac{Gr}{(n_2^2 - n_6^2) \frac{\partial \theta_1}{\partial y} \frac{Gc}{(n_4^2 - n_6^2) \frac{\partial \phi_1}{\partial y}}} \right]$$

(31)

$$Nu = - \left(\frac{\partial \theta}{\partial y} \right)_{y=h_1, h_2} = -\varepsilon [e^{ti} (a_{11} n_2) e^{n_2 y} - (a_{12} n_2) e^{-n_2 y}] + (a_{01} n_3) e^{n_3 y} - (a_{02} n_3) e^{-n_3 y} \quad (32)$$

$$Sh = - \left(\frac{\partial \phi}{\partial y} \right)_{y=h_1, h_2} = -\varepsilon [e^{ti} (b_{11} n_4) e^{n_4 y} - (b_{12} n_4) e^{-n_4 y}] + b_{01} n_5 e^{n_5 y} - b_{02} n_5 e^{-n_5 y} \quad (33)$$

All the constants appearing in the above solutions are given below:

$$\begin{aligned} n_2^2 &= Q + i Pr \omega; n_3^2 = Q; n_4^2 = KSc - i\omega Sc; n_5^2 = KSc; \\ n_6^2 &= s^2 + M^2 + i\omega; n_7^2 = s^2 + M^2; \\ a_{01} &= \frac{-e^{-2n_3}}{1 - e^{-2n_3}}; a_{02} = \frac{1}{1 - e^{-2n_3}}; a_{11} = \frac{-e^{-2n_2}}{1 - e^{-2n_2}}; a_{12} \\ &= \frac{1}{1 - e^{-2n_2}}; \\ b_{01} &= \frac{-e^{-2n_5}}{1 - e^{-2n_5}}; b_{02} = \frac{1}{1 - e^{-2n_5}}; b_{11} = \frac{-e^{-2n_4}}{1 - e^{-2n_4}}; b_{12} \\ &= \frac{1}{1 - e^{-2n_4}}; \\ c_{01} &= \left\{ 1 + \frac{Gr}{(n_3^2 - n_7^2) \frac{Gc}{(n_5^2 - n_7^2) \frac{M^2}{n_7^2}}} \right\} \left(1 - \frac{e^{n_7}}{A} \right) \frac{M^2}{An_7^2} \end{aligned}$$

$$c_{02} = \left\{ 1 + \frac{Gr}{(n_3^2 - n_7^2) \frac{Gc}{(n_5^2 - n_7^2)} \frac{M^2}{n_7^2}} \right\} \left\{ \left(\frac{e^{n_7}}{A} \right) \frac{M^2}{An_7^2} \right\}$$

$$c_{11} = \left\{ 1 + \frac{Gr}{(n_2^2 - n_6^2) \frac{Gc}{(n_2^2 - n_6^2)} \frac{M^2 + i\omega}{n_6^2}} \right\} \left\{ \left(1 - \frac{e^{n_6}}{B} \right) \frac{M^2 + i\omega}{Bn_6^2} \right\}$$

$$c_{12} = \left\{ 1 + \frac{Gr}{(n_2^2 - n_6^2) \frac{Gc}{(n_2^2 - n_6^2)} \frac{M^2 + i\omega}{n_6^2}} \right\} \left\{ \left(\frac{e^{n_6}}{B} \right) \frac{M^2 + i\omega}{Bn_6^2} \right\}$$

$$A = 2 \sinh(n_7); \quad B = 2 \sinh(n_6)$$

Results and Discussion

The results of the above problem discussed with the graphs drawn for the impact of parameters on various profiles of flow field.

Velocity Profiles

In fig.1, the impact of Grashoff number (Gr) on velocity (u) is presented. As Gr increases velocity increases. From fig.2, the mutual effect of three parameters (ω , Gr) and K oscillation frequency (ω), Grashoff number (Gr) and chemical reaction parameter (K), on velocity (u) can be observed.

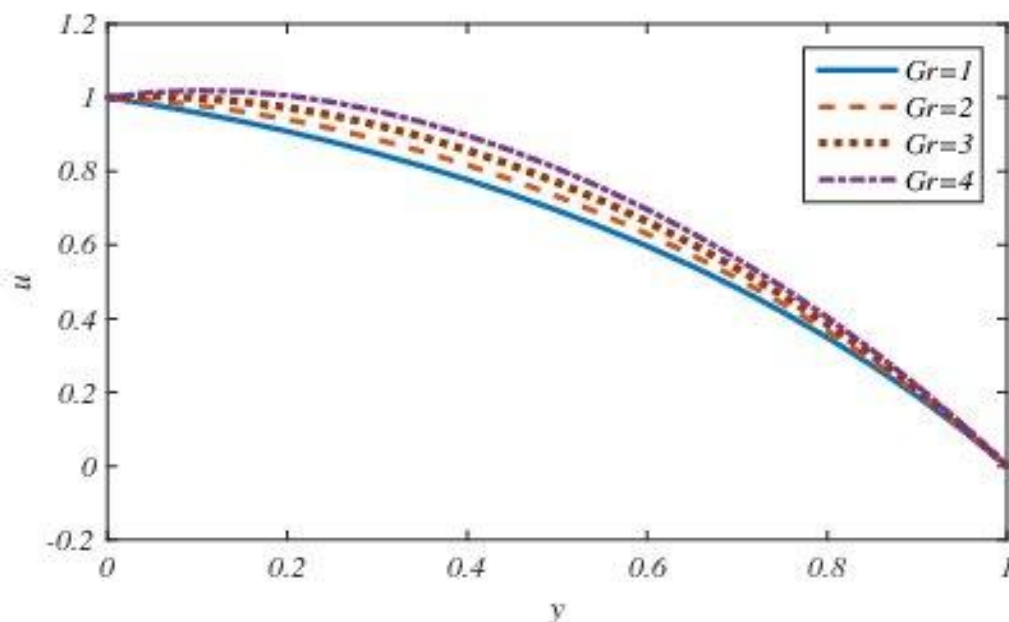


Figure 1. Influence of Grashoff number (Gr) on velocity for $\omega = 2$, $Pr = 0.71$, $t = \pi/2$, $q = 0.1$, $K = 1$, $Sc = 0.6$, $M = 2$, $s = 1$, $Gc = 1$, $Q = 1$

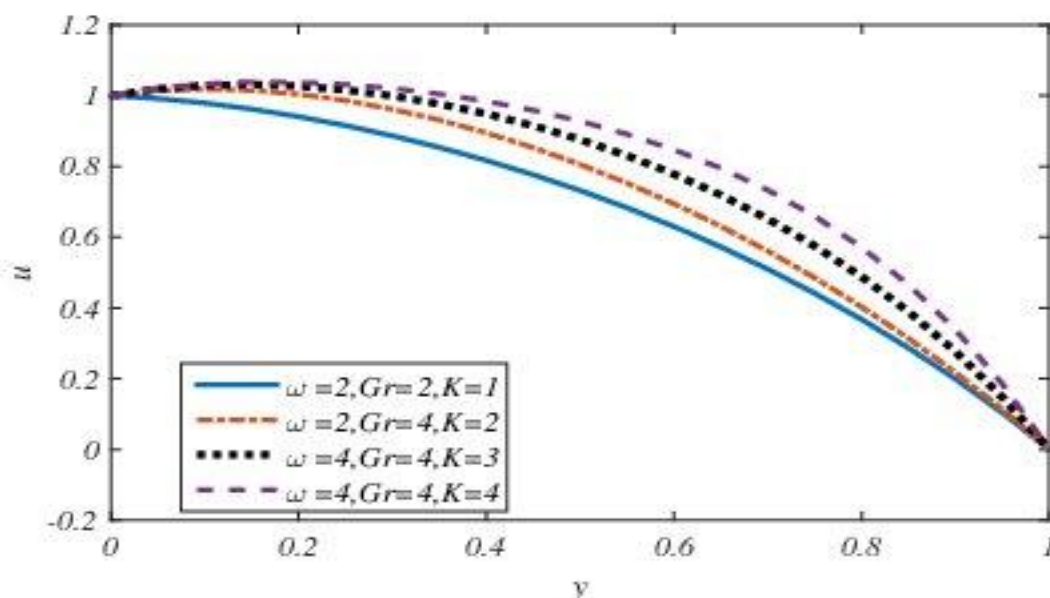


Figure 2. Influence of Gr, K, ω on velocity for $M = 2, Pr = 0.71, t = \pi/2, \varepsilon = 0.1, K = 1, Sc = 0.6, M = 2, s = 1, Gc = 1, Q = 1$

When $\omega = 2$, Gr increasing from 2 to 4 and increasing from 1 to 2 simultaneously, velocity increases. But for $\omega = 4, Gr = 4$ and chemical reaction K increases from 3 to 4, only little variation in velocity has been observed. As the parameter M increases, velocity decreases as shown in fig.3.

The combined effect of parameters Gr, ω and M on velocity is depicted in the fig.4. For $M = 2$, when ω increasing from 1 to 2 and Gr increasing for 2 to 4, velocity increases. When $M = 4$, each of ω and Gr increasing from 2 to 4, velocity showing only marginal increase.

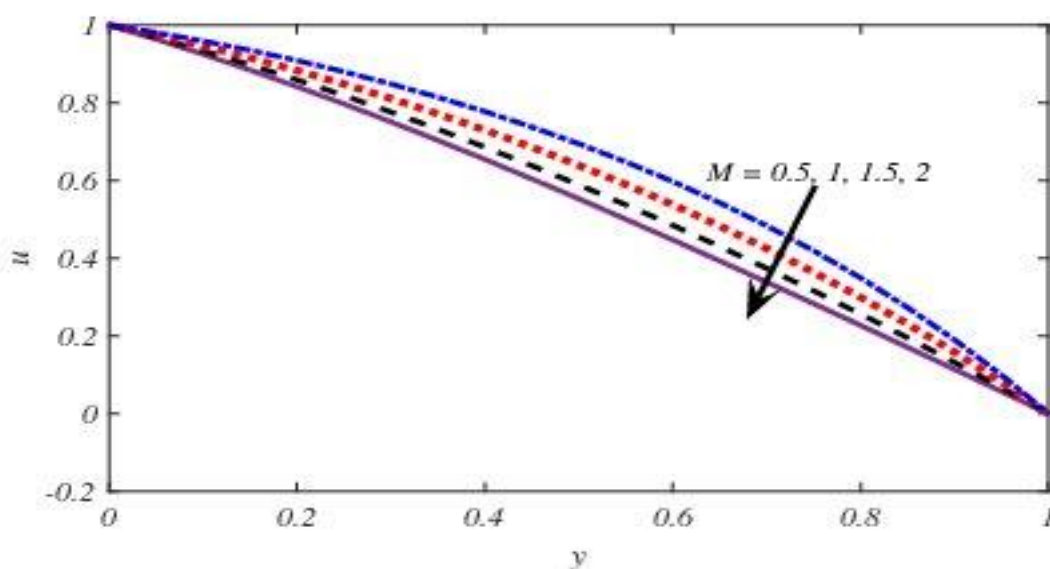


Figure 3. Influence of M on velocity for $\omega = 2, Pr = 0.71, t = \pi/2, \varepsilon = 0.1, K = 1, Sc = 0.6, s = 1, Gc = 1, Q = 1$

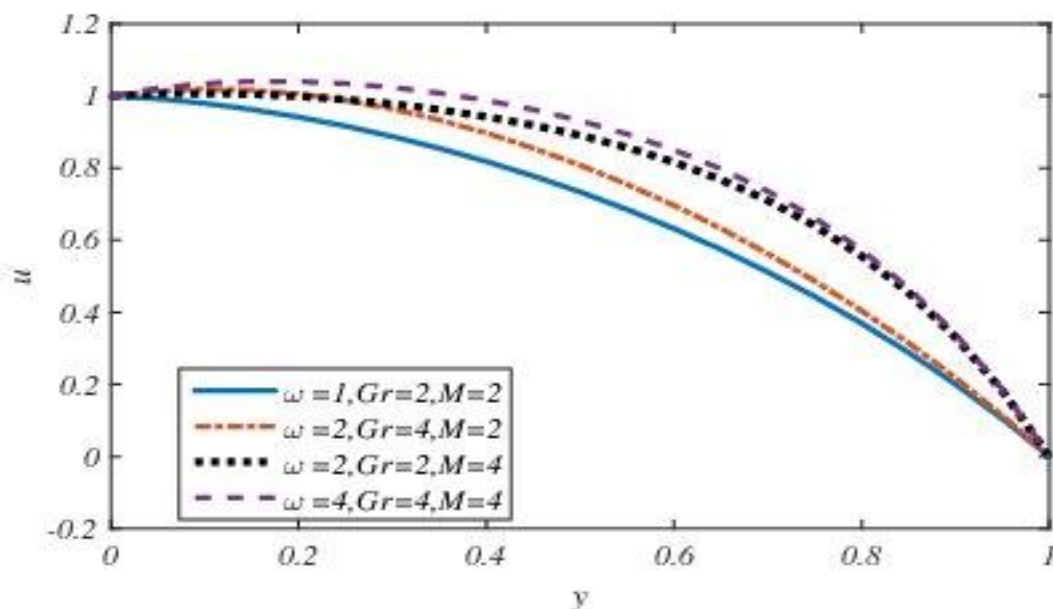


Figure 4. Influence of Gr, M, ω on velocity for $Pr = 0.71, t = \pi/2, \varepsilon = 0.1, K = 1, Sc = 0.6, s = 1, Gc = 1, Q = 1$

Temperature Profiles

In fig.5, influence of ω on temperature (θ) is presented. As ω increases, temperature (θ) also increases. As Prandtl number (Pr) increases from 0.7 to 3.7, temperature (θ) decreases as shown in fig.6. In fig.3.8, as (Q) increases, it is observed that temperature (θ) also increases.

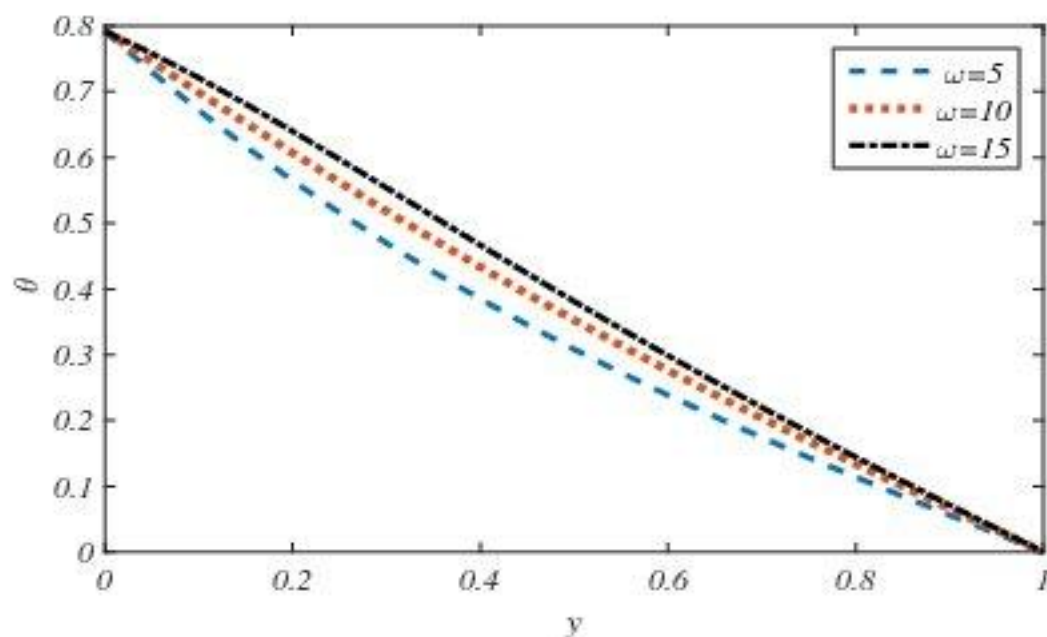


Figure 5. Influence of oscillation frequency (ω) on Temperature for $Q = 4, \varepsilon = 0.1, Pr = .7, t = 2$

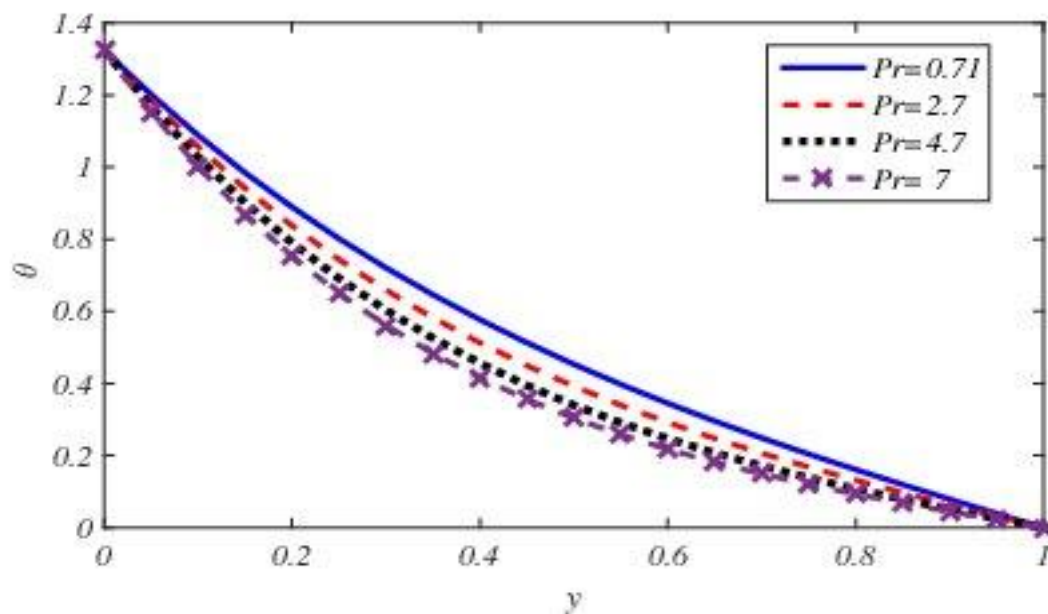


Figure 6. Impact of Pr on θ for $Q = 3$, $t = 1.6$, $\omega = 3$, $\varepsilon = 0.1$

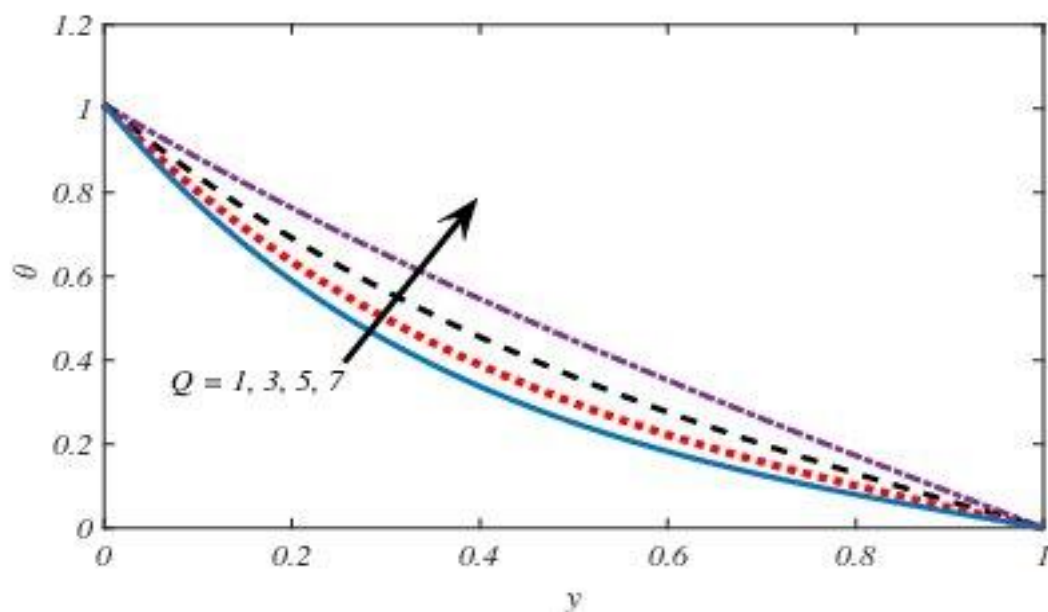


Figure 7. Influence of Q on Temperature for $\omega = 2$, $Pr = 2.7$, $t = .2$, $\varepsilon = 0.1$

Concentration Profiles

Fig.8 – fig.9 reveal that concentration (ϕ) decreases when the chemical reaction parameter (K) and oscillation frequency (ω) increases.

Variation in concentration (ϕ) observed to be small for values of K around 2, compared to the variations for values of K , around 1.

In fig. 10, as Schmidt number (Sc) increases concentration (ϕ) decreases.

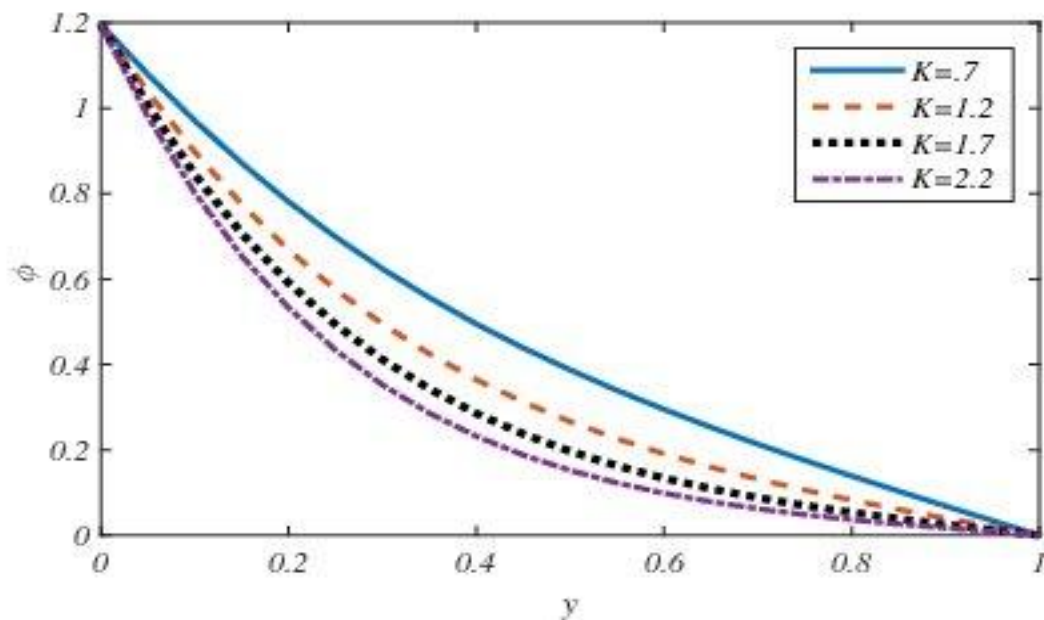


Figure 8. Influence of K on Concentration for $\omega = 6$, $t = .2$, $\varepsilon = 0.1$, $Sc = 4$

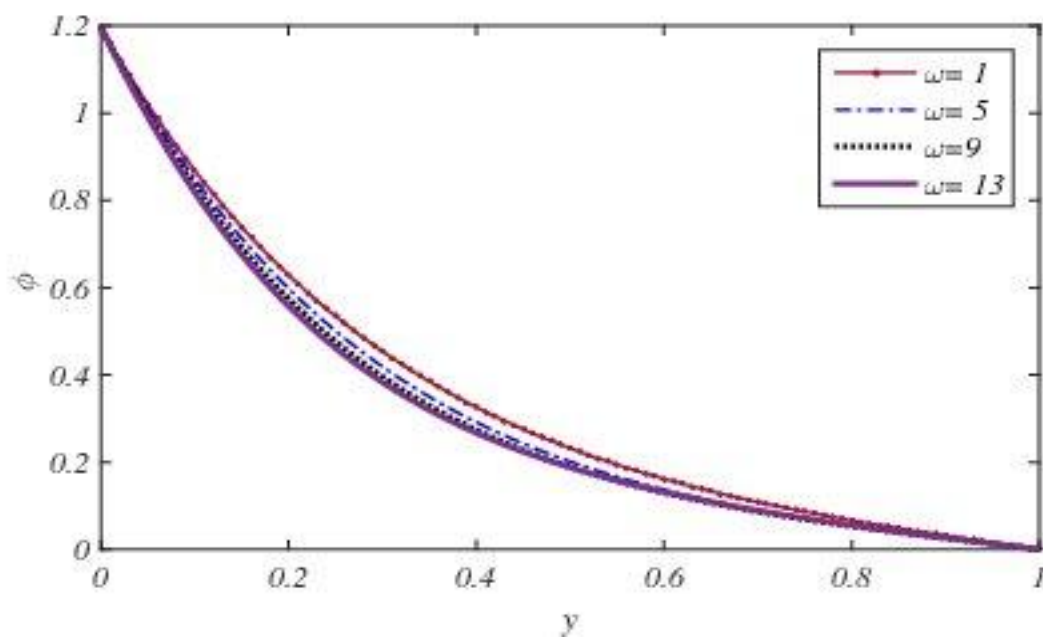


Figure 9. Influence of oscillation frequency (ω) on Concentration for $K = 2$, $t = .1$, $\varepsilon = 0.1$, $Sc = .74$

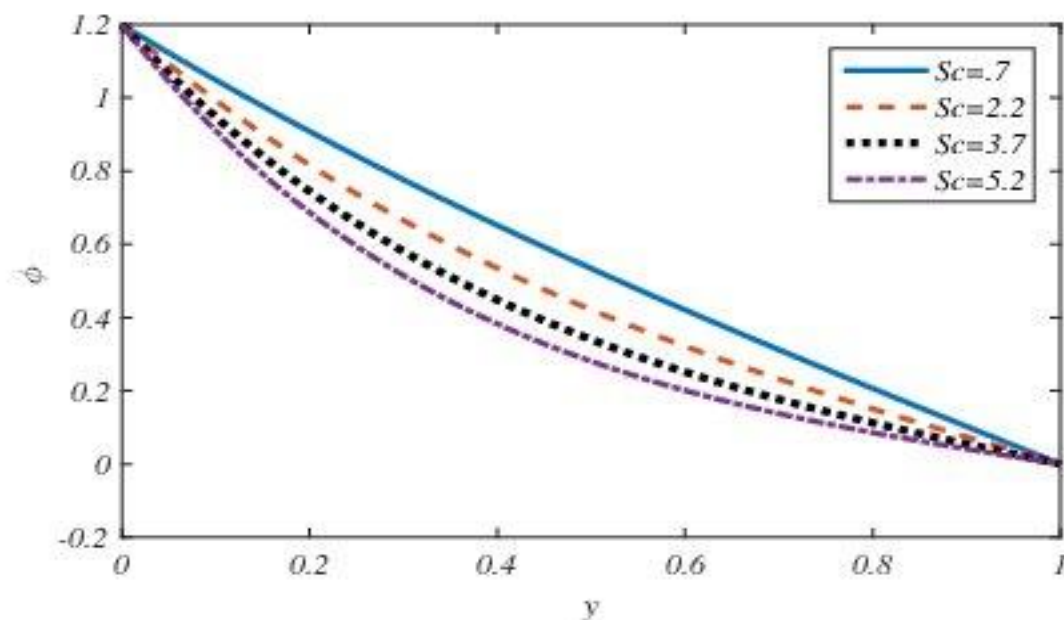


Figure 10. Influence of Sc on Concentration for $K = 1.3$, $\omega = 2$, $t = .1$, $\varepsilon = 0.1$

Skin Friction

Fig.11, reflects the influence of Grashoff number (Gr) on skin friction (τ) along the boundaries. As Gr increases, skin friction (τ) increases at both the plates $y = 0$ and $y = 1$. Fig.12 shows the influence of Hartmann number (M) on skin friction (τ). As M increases, skin friction (τ) decreases uniformly at both the plates $y = 0$ and $y = 1$.

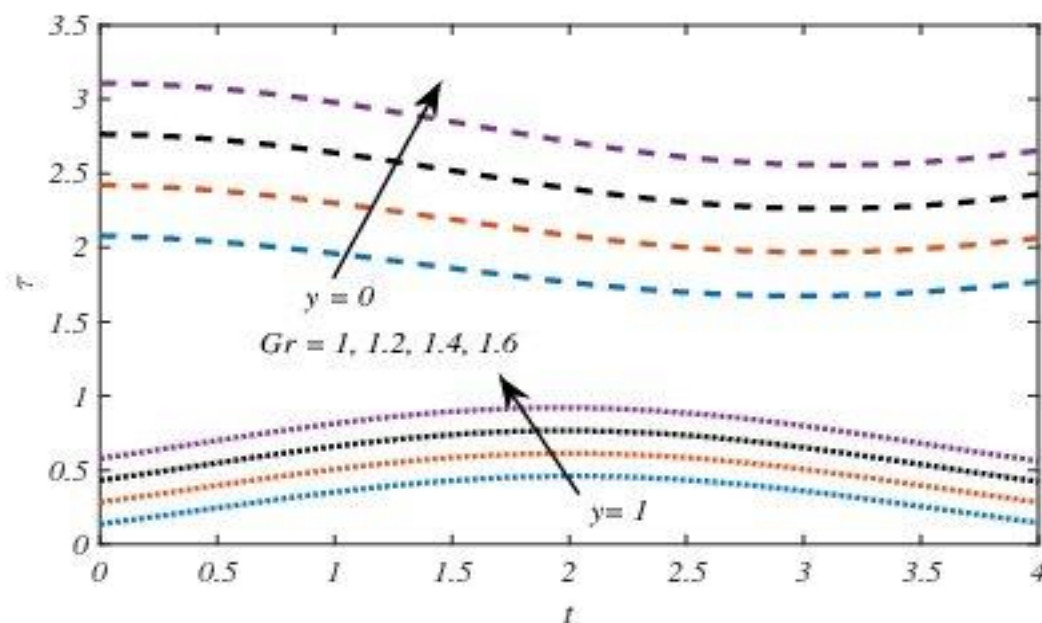


Figure 11. Influence of Gr on τ for $Q = 1$, $\omega = 4$, $\varepsilon = 0.1$, $K = 1$, $Sc = 0.9$, $M = 1$, $s = 1$, $Pr = 0.71$, $Gc = 1$

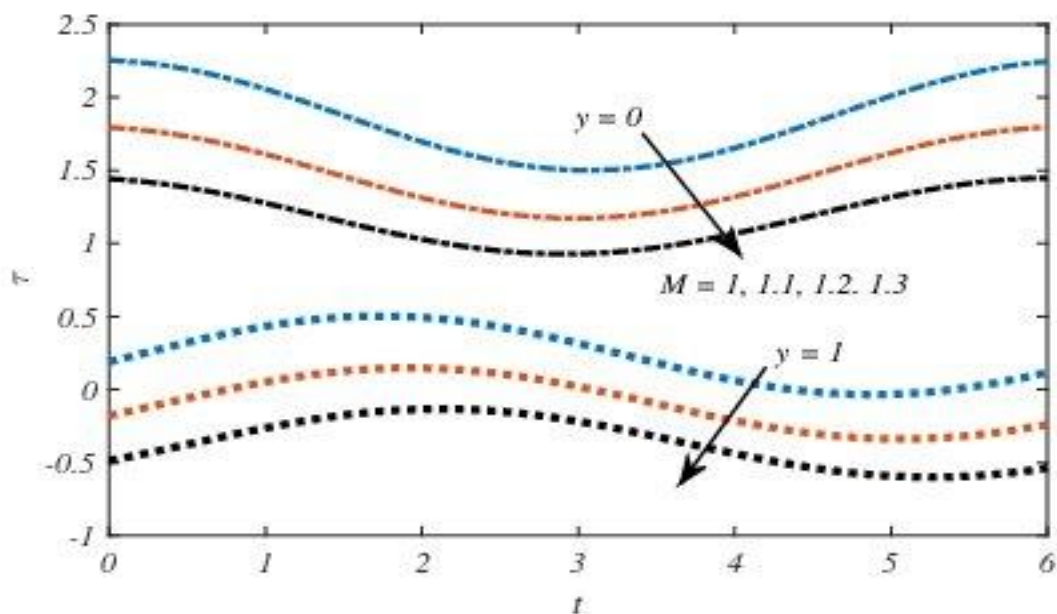


Figure 12. Influence of M on τ for $Q = 1$, $\omega = 2$, $\varepsilon = 0.1$, $K = 1$, $sc = 0.9$, $s = 1$, $Gr = 1$, $Gc = 1$, $Pr = 0.71$

Heat Transfer

As oscillation frequency (ω) increases, the Nu decreases for the range $y = 0$ (left plate) to $y = 0.4$ (nearer to half the distance) and then for $y = 0.4$ to $y = 1$ (right plate), Nu increases, as shown in fig.13.

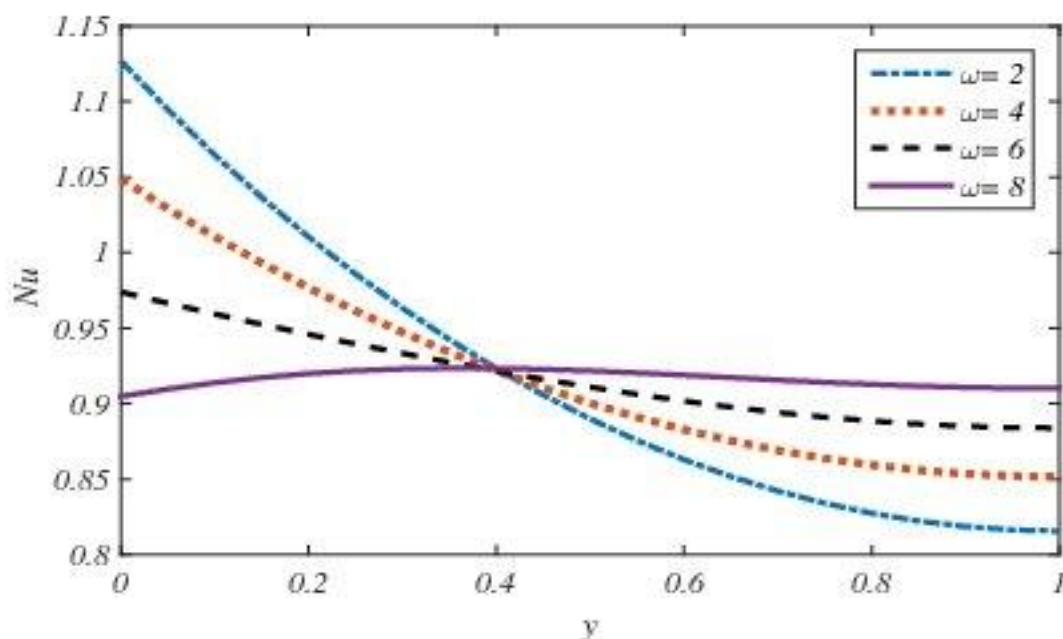


Figure 13. Influence of oscillation frequency (ω) on Heat transfer for $Q = 1$, $Pr = .7$, $\varepsilon = 0.1$, $K = 1$, $Sc = .5$, $s = 0.2$, $Gr = 1$, $Gc = 1$, $M = 3$, $t = 2$

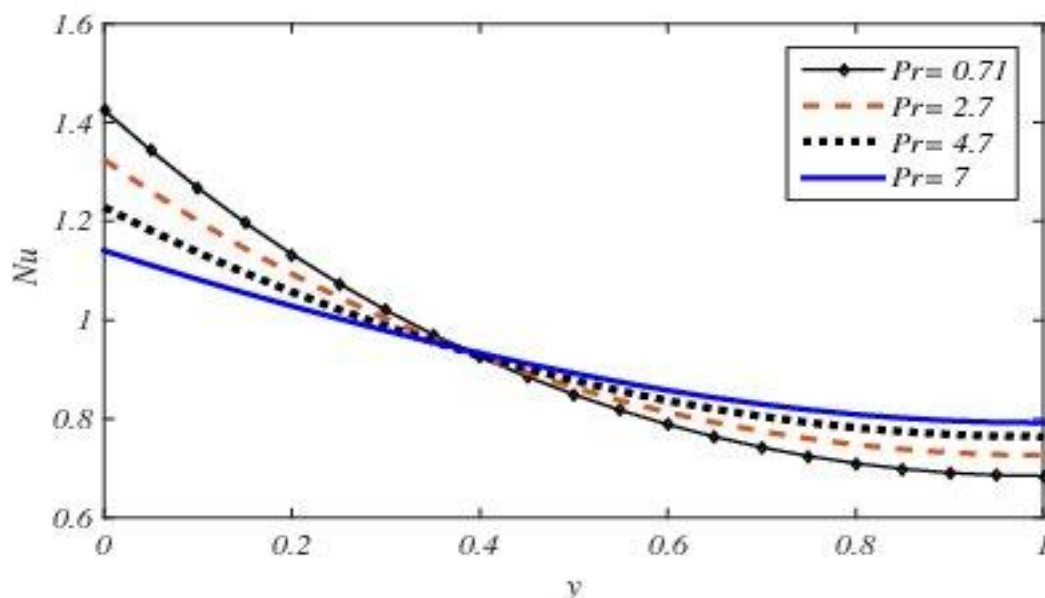


Figure 14. Influence of Prandtl number (Pr) on Heat transfer for $Q = 1$, $\varepsilon = 0.1$, $K = 1$, $Sc = .5$, $s = 0.2$, $Gr = 1$, $Gc = 1$, $M = 3$, $t = 2$

Mass Transfer

In fig.14, for the increase in chemical reaction parameter (K), Sherwood number (Sh) initially increases for $y = 0$ to $y = 0.4$ and then for $y = 0.4$ to $y = 1$, the pattern is reversed.

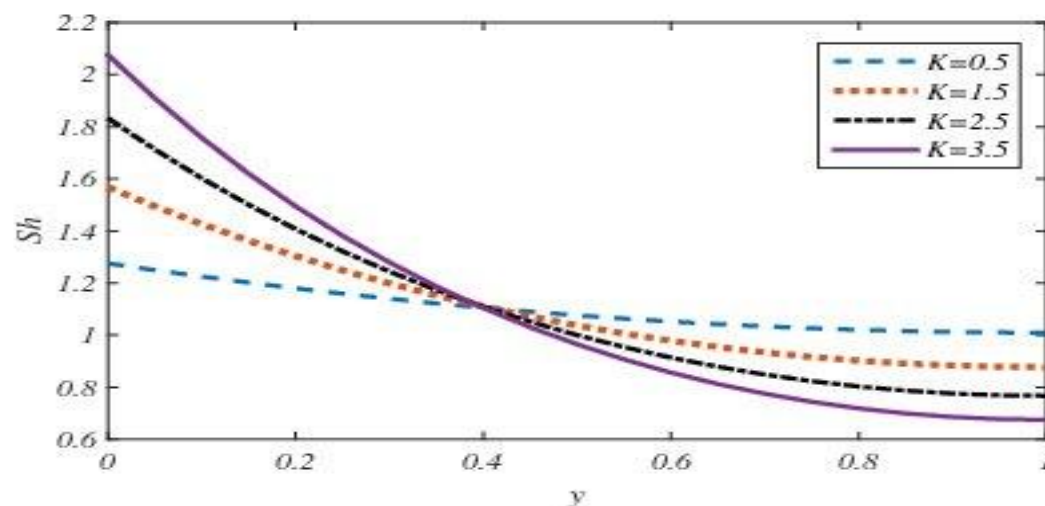


Figure 15. Influence of K on Mass Transfer for $\omega = 2$, $t = .2$, $\varepsilon = 0.1$, $Sc = 0.9$

Conclusion

Analysis of this problem involves exploring the influence of chemical reaction (K) and heat source (Q) on various profiles of MHD oscillatory Couette flow as highlighted below.

1. The mutual impact of Grashoff number (Gr), frequency of oscillation (ω) and chemical reaction (K) results in the enhancement of velocity (u). Values of Gr , ω and K with high magnitude reduces variation in velocity (u).
2. Increase in Hartmann number (M) reduces velocity (u) as well as skin friction (τ) at the walls.

3. Increment in Grashoff number (Gr) results in the enhancement of velocity (u) between the walls and skin friction (τ) rise at both the walls.
4. Increase in Q (or) ω , increases the temperature (θ).
5. Impact of Prandtl number (Pr) diminishes the temperature (θ).
6. Concentration reduces due to the impact of each of the parameters K, ω and Sc.
7. Nusselt number (Nu) oscillates for the increase in frequency of oscillation (ω) and Sherwood number (Sh) oscillating for increase in chemical reaction (K).

References

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